Steam Thermocompressor Systems

INTRODUCTION
With today’s rising fuel costs and the immediate need to not vent steam systems to the atmosphere, steam plants are reviewing the operation and application of steam thermocompressor technology to recover low-pressure steam that is not required for use in the process plant. Many industrial plants are looking at the different steam thermocompressing applications to improve the steam system balance.

THERMOCOMPRESSORS DEFINED
A thermocompressor is a device that uses high-pressure steam as a motive force to entrain a lower-pressure steam, then discharge the mixture at an intermediate steam pressure. Integrating the device correctly into the steam and condensate system can save the plant a tremendous amount of energy and reduce emissions. The technology has been used for many years in several industries.

TYPES OF THERMOCOMPRESSING UNITS
These units are simple, versatile, and can be applied in many different steam process applications. They have few moving parts and have a relatively low cost for implementation into the steam system. Thermocompressors typically used in steam operations generally include one of these design features: fixed-nozzle, automatically controlled spindle, or variable orifice.

CONSTRUCTION AND OPERATION
A thermocompressor is used to recover the latent heat content of the low-pressure suction steam to produce an intermediate steam pressure for use in the industrial plant. An ejector is a unit used to create a vacuum in a process application. The ejector operation will typically contain non-condensable gases, which makes it difficult to recover the heat energy from the suction vapor.

However, thermocompressors and ejectors operate on the same thermodynamic and physical principles. One is that some of the energy contained in high-pressure steam can be transferred to a lower-pressure vapor or gas to produce a mixed discharge stream.
of intermediate pressure. The only difference is the objective.

The components of a thermocompressor are as follows:
1. Body
2. Diffuser
3. Nozzle
4. Spindle
5. Actuator to move the internal spindle

The motive steam leaves the nozzle at high velocity (1,500 to 2,500 ft./s). High-pressure motive steam is delivered at a very high velocity through a converging diverging nozzle, where it comes into contact with the low-pressure steam, resulting in the entrainment and mixing.

High-pressure inlet motive steam is expanded in the nozzle to the suction chamber, where the pressure energy is converted to velocity energy. The mixed jet flow stream is then forced through a diffuser, where the kinetic energy is converted into potential energy. Steam compression is achieved through converting potential or pressure energy into kinetic energy and then back into pressure energy. The name thermocompressor is derived from the process of using thermal energy, or the enthalpy of steam, to achieve compression.

A thermocompressor requires engineering to balance the steam flow streams, including a determination of the correct steam flow and steam pressure of the motive steam, suction, and intermediate steam. An incorrect balance of the steam flows could result in choke flow conditions, and an increase in motive steam could lower the suction steam flow.

A steam line separator takes advantage of the inertia difference between condensate (liquid) and steam (vapor). The design of the separator will determine the required pressure drop across the separator, and it’s that pressure drop that creates the velocities required to separate the moisture from the steam flow. Here are nine important items to consider when selecting a separator:

**CRITICAL OR NONCRITICAL PERFORMANCE**

The performance of a thermocompressor is categorized as either critical or noncritical based on the compression ratio. The compression ratio is defined as the discharge absolute steam pressure divided by the suction absolute steam pressure: ratio = P2/Ps (absolute units).

**Critical**

If the steam velocity in the diffuser throat is sonic, the design is defined as critical. Sonic velocity exists when the compression ratio (discharge pressure/suction pressure) is equal to or greater than 1.8 to 1. The value of this ratio changes as a function of the ratio of the specific heat of the motive and suction steam.

**Noncritical**

The other type of performance is termed noncritical and does not require sonic velocity in the diffuser to achieve the desired compression. A thermocompressor operating where the steam velocity is subsonic or noncritical has a discharge/suction ratio pressure of less than 1.8 to 1. The motivating steam pressures can be changed, and discharge steam pressure will cause gradual changes in both suction pressure and capacity. Lower capacities can be obtained by throttling the motive steam pressure.

A high percentage of steam system installations operate in the noncritical mode. The suction flow varies directly with the motive steam flow at a given discharge pressure. If the motive steam flow increases and additional suction flow is not available, the differential pressure will increase until equilibrium is established.
SIZING A UNIT
The performance of a steam thermocompressor is generally evaluated for several anticipated operating conditions, but normally a minimum and maximum operating point are sufficient. To properly size the unit, the thermocompressor requires the following design data:

1. Motive steam pressure
2. Motive steam temperature
3. Suction steam pressure
4. Suction steam flow
5. Discharge steam pressure

The calculations are then made on maximum-minimum conditions, and a thermocompressor design is determined. At higher motive steam pressures, the entrainment ratio tends to be lower for the same compression ratio. Typically, thermocompressors are feasible for low compression ratios (2.5), while for higher compression ratios, the complete steam balance must be evaluated to arrive at a suitable solution due to the increased entrainment ratio requirement. Typical entrainment ratios vary between 1.5 and 3 and depend on expansion as well as compression ratios.

STEAM THERMOCOMPRESSION APPLICATIONS
There are many appropriate applications for steam thermocompressor systems in today’s industrial plant operations:

Thermocompressing Flash Tank Systems
The thermocompressor uses high-pressure motive steam to remove low-pressure flash steam from the flash tank and deliver it to an intermediate steam pressure. A very simple control loop consumes low-pressure steam and provides a more useful steam pressure for the processes.

Recirculating Loop Thermocompressor System
The recirculating loop system consumes the flash steam off the condensate discharge of the process application, which can be of any process type: rotating dryer, heat exchanger, reboiler, process air unit, etc. The thermocompressor, using high-pressure steam as
the motive force, consumes the flash steam off the flash tank and provides a usable steam pressure back to the inlet of the process steam supply. A make-up valve provides the additional steam to maintain the process requirements for steam energy. The recirculating loop system is a very efficient method for steam balancing a process application.

**Steam Balancing System**

The steam balancing thermocompressor system uses unnecessary low-pressure steam by using the higher-pressure steam as the motive force and developing an intermediate steam pressure. This prevents the venting of low-pressure steam that has no applications in the plant’s processes.

![Steam Balancing System Diagram](image-url)